# Pickering emulsions synthesized from iron oxide nanocolloids and used as agents for the residual oil displacement in porous media

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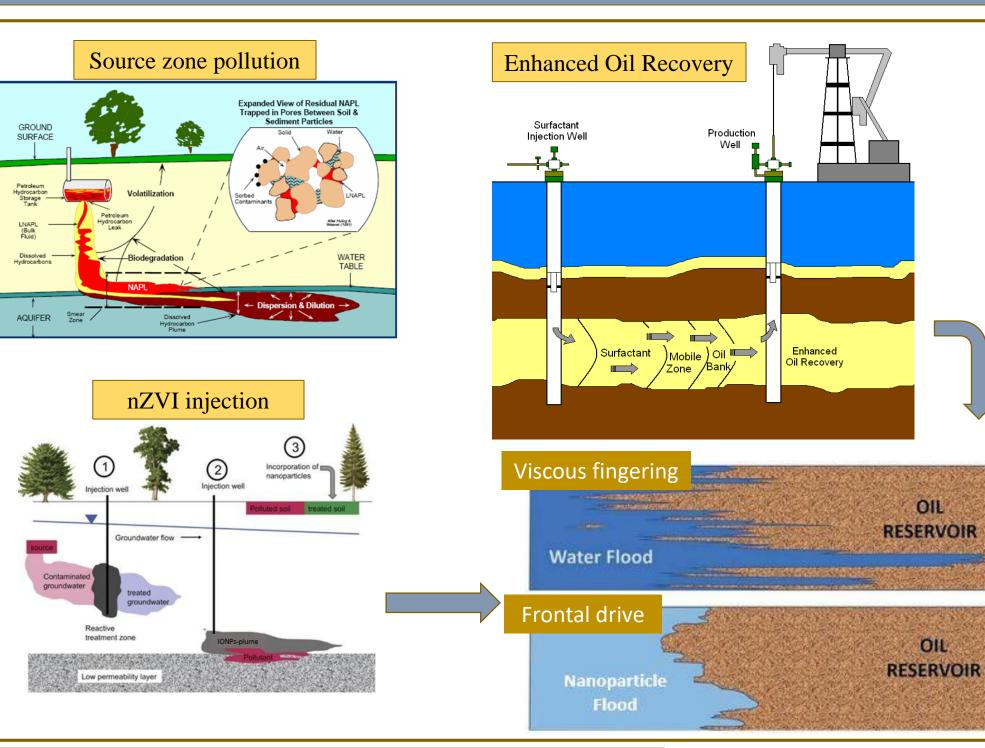


INSTITUTE OF CHEMICAL ENGINEERING SCIENCES



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suspensions of non-oxide nanoparticles non-polluted sons.	of vadoze / saturated zones of the subsurface, and energy production like the enhanced oil recovery from oil-bearing reservoir rocks. The remediation of soils polluted by non- aqueous phase liquids (NAPLs) resulting from leaking storage tanks, spills and improper waste disposal is considered as one of the most significant challenges. NAPLs have caused widespread subsurface contamination, while they tend to sink in groundwater systems, resulting in complex dispersal and plume patterns, which are long-term sources of subsurface pollution, and difficult to clean-up. Moreover, the continuous dissolution of NAPLs may lead to the extensive contamination of groundwater. Concerning energy production, due to population and economic growth, the global energy consumption is estimated to increase by almost 50% in the next thirty years. The overall oil recovery efficiency for primary and secondary recovery range from 35% to 45% and tertiary recovery methods that can increase the enhanced oil recovery (EOR) efficiency by 10-30% could contribute to energy supply. Conventional methods include chemical flooding, gas injection, thermal recovery, microbial enhanced oil recovery (MEOR), low-salinity waterflooding, and foam-EOR. Chemical EOR (CEOR) includes different methods of injecting polymers, surfactants, alkaline, emulsions, and foams.	<ul> <li>Correlation of the stability / longevity of nano-colloids, and rheological behavior of Pickering emulsions with their composition (salinity, ionic strength, oil to water volume ratio).</li> <li>Correlation of the interfacial and rheological properties of "smart fluids" with their capacity to mobilize oil ganglia from porous media (micromodels, sandpacks).</li> </ul>

#### **Oil recovery from subsurface and reservoir rocks**



Secondary

Imbibition

S

0.50

0.518

0.45

Total Oil

recovery

efficiency

(%)

41.2

38.3

44.4

#### Synthesis and stabilization of nano-colloids

Polyphenol-co	oated iron oxide nanoparticles (IONPs)
<image/> <section-header></section-header>	<image/>

FeCl <sub>3</sub> 0.1M	
IONP suspension	<b>IONP Synthesis</b>

 $\langle \mu \rangle =$ 

Average viscosity vs time

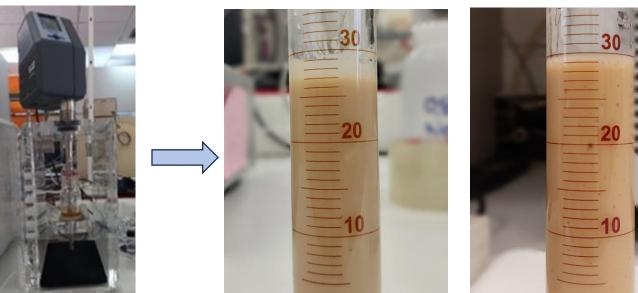
- C<sub>Fe</sub>=0.75g/L

▲ C<sub>Fe</sub>=0.5g/L 

100

Time,t (s)

### **Synthesis and Properties of Pickering Emulsions**



The rheology of Pi	ckering emulsions follows the
power law model:	$\mu = \mu_{inf} + (\mu_1 - \mu_{inf})\dot{\gamma}^{n-1}$
$\int_{\mu_1} - \mu_{inf}$	$1 \qquad 1 \qquad 1 \qquad \leq 1 > \qquad \leq 1$

**PPH** extract

$\mu_{inf} + \left(\frac{\mu_1 - \mu_{inf}}{n}\right) \gamma_w^{n-1}$	$Ca = \frac{u_0 < \mu > 1}{2}$
	$\gamma_{ow}$

0.35

0.30 -

0.25 ج

Densi

0.15

0.10 -

0.05 -

	1.00	
$\gamma_w = \left(\frac{8u_p}{4r_H}\right) \left(\frac{3n+1}{4n}\right) \rightarrow$	$u_p = \frac{u_0}{\varphi_V} \rightarrow \varphi_V = \frac{\pi \langle W_p \rangle \langle D_p \rangle}{4L_p^2}$	

Oil-drop size distributions in emulsions

Diameter (um)

2.2

 0.75
 2.8
 0.8

 0.5
 4.9
 1.9

 0.25
 7.9
 2.3

K =

 $\mu_{oil}$ 

#### **Properties of Iron Oxide Nanoparticles (IONPs)**

	PPHs : pH = 6.36 , ζ-potential = -37.7mV IONPs : pH = 6.05 , ζ-potential = -22.9mV				
Vanoparticle suspension	Surface tension (mN/m)	Interfacial tension (mN/m)	Contact angle air / suspension θ(°)	Contact angle synthetic oil / suspension θ(°)	Average diameter of nanoparticles (nm)
ONPs 1.0g/L	52.89±0.29	53.54	21.7 ± 0.02	9.6± 8.7	141.8±5.8
ONPs 0.75g/L	54.47±0.41	55.31	25.7 ± 0.20	20.7 ± 5.1	164.2±2.2
ONPs 0.5g/L	56.48±0.27	58.12	33.4 <u>+</u> 2.4	24.9 <u>+</u> 3.1	105.7±8.2
ONPs 0.25g/L	59.78±0.17	58.35	25.4±1.20	19.1±0.6	105.7±16.2
PPHs 3.0g/L	45.29 ±0.13	49.05	-	-	68.06±8.3

During processes, the physicochemical properties of the rock alter to favor the mobilization of trapped oil ganglia. This might occur with: (i) the reduction of the interfacial tension thus increasing the capillary number; (ii) the increase of water viscosity, thus increasing the mobility ratio; (iii) the alteration of the wettability, thus facilitating the detachment of oil from the rock surfaces.

	Emulsion	μ <sub>1</sub> (Pa s)	μ <sub>inf</sub> (Pa s)	п	<µ> (Pa s)	Ca (10 <sup>-5</sup> )	К
	$C_{\rm Fe} = 1.0 \ g/L$	2.468	0.001	0.196	0.423	11.9	1.63
1	$C_{\rm Fe} = 0.75 \ g/L$	1.053	0.003	0.217	0.189	5.98	0.72
	$C_{\rm Fe} = 0.50 \ g/L$	0.213	0.006	0.252	0.045	1.37	0.17
	$C_{\rm Fe} = 0.25 \ g/L$	0.564	0.002	0.287	0.115	3.45	0.44

IONPs 0.25g/L	0.81	0.53	0.52	35.8
PPHs 3.0g/L	0.82	0.542	0.541	34.0

Suspension of iron-oxide nanoparticles (IONPs) as

injection fluid in Secondary Imbibition

Primary

Imbibition

S

0.52

0.511

0.45

Primary

Drainage

S<sub>o</sub>

0.85

0.84

0.81

Nanoparticle

suspension

IONPs 1.0g/L

IONPs 0.75g/L

IONPs 0.5g/L

Experimental tests in glass etched pore network with nanoparticle suspensions at various concentrations gave the aforementioned residual oil saturation values per each cycle, namely Primary Drainage (oil displaces water), Primary Imbibition (water displaces oil) and Secondary Imbibition (nanoparticle suspension displaces oil). The changes of oil saturation between primary and secondary imbibition tests are quite small, thus the potential to stabilize Pickering emulsions and use them as injection fluids in Secondary Imbibition was investigated.

For assessing emulsions: (1) their stability is quantified by the macroscopic- phase separation and microscopic oil-drop size distribution; (2) the shear viscosity is measured as function of time with steady-state tests, and the loss and storage moduli are measured with dynamic frequency sweep tests on a stress rheometer.



Emulsion stability vs time

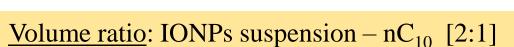
Time,t (min)

(a) C<sub>fe</sub> = 0.25g/L (b)  $C_{fe} = 1.0g/L$ **IONP stabilized Pickering emulsions** 

s)

(Pa

**Ultrasound probe** 

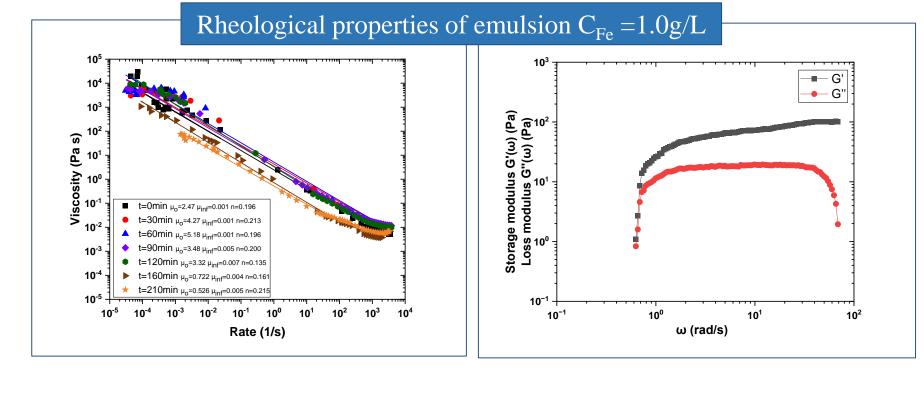


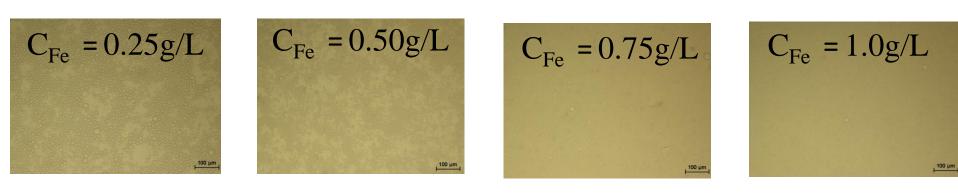
----- C<sub>Fe</sub> = 0.75g/L

▲ C<sub>Fe</sub> = 0.5 g/L

▼ C<sub>Fe</sub> = 0.25 g/L

 $\gamma_w$  is the shear rate at pore-wall,  $\varphi_V$  is the porosity of the planar porous medium at the vertical direction,  $r_{H}$  is the equivalent hydraulic pore radius ( $r_H$ =45 µm) [3], Ca is the capillary number,  $\kappa$  is the viscosity ratio ,  $\mu_{oil} = 0.026$  Pa s

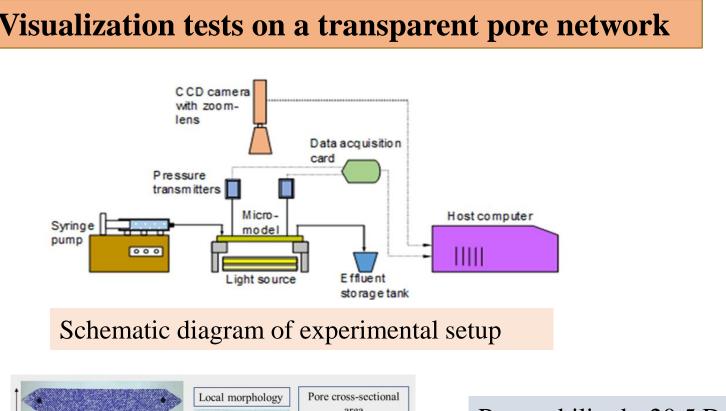


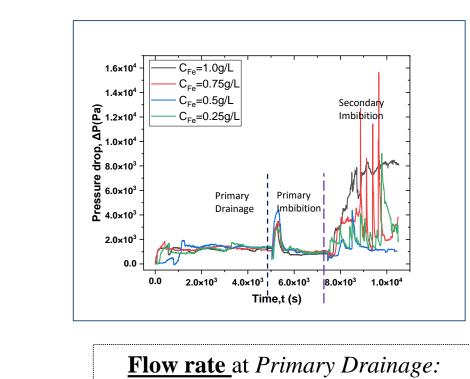


## Assessing the displacement efficiency of Pickering emulsions

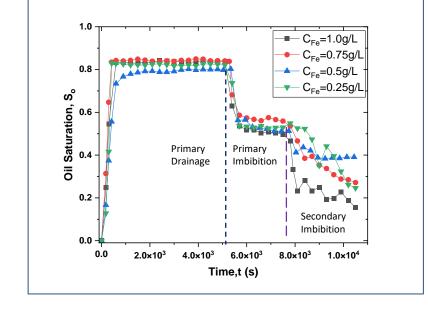
200

150





0.08mL/min



**Injected Volume** Primary Drainage: 8mL Primary Imbibition: 8mL

